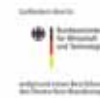


Continuous Reduction of Hardly Water-Soluble Ketones with an Ionic Liquid as Solubiliser

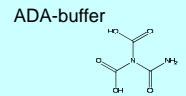
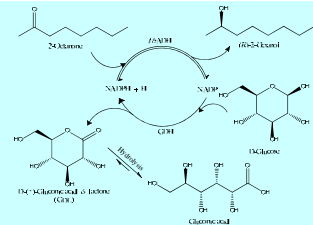
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Period: 01.10.2010 – 31.12.2011



Introduction

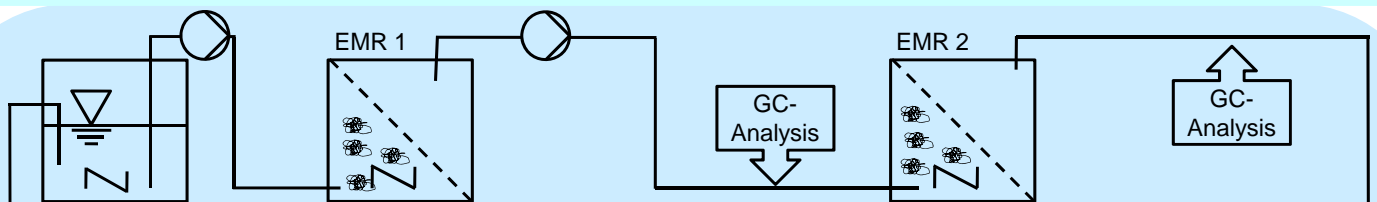
1. The enantioselective reduction of hardly water-soluble ketones is carried out with an alcohol dehydrogenase from *Lactobacillus brevis* (LbADH).
2. Cofactor Regeneration is performed with a Glucose dehydrogenase (GDH).
3. To overcome solubility restrictions of long-chain ketones (2-octanone and 2-nonanone), the ionic liquid (TEGO IL K5) is used as solubiliser.
4. The continuous synthesis of the corresponding (*R*)-2-alcohols is carried out in an enzyme membrane reactor (EMR) and in a reactor cascade (two EMR).
5. The isolation of the ketone and alcohol is feasible via solid phase extraction (SPE) and subsequent elution with *n*-heptane.
6. The reaction mixture can be recycled and is re-used as substrate solution.



Reaction System used for the production of (*R*)-2-alcohols

Ionic Liquid TEGO IL K5

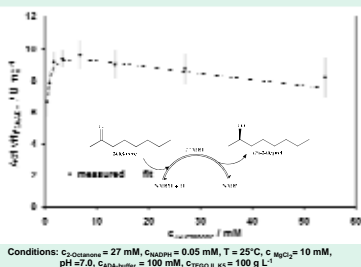
Continuous Synthesis of (*R*)-2-alcohols



Kinetic measurements in a Multiplate-reader



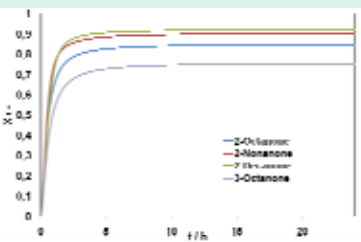
Extended Michaelis-Menten-Model



Conditions: $C_{2\text{-Octanone}} = 27 \text{ mM}$, $C_{\text{NADPH}} = 0.05 \text{ mM}$, $T = 25^\circ\text{C}$, $C_{\text{H}_2\text{O}_2} = 10 \text{ mM}$, $\text{pH} = 7.0$, $C_{\text{ADA-buffer}} = 100 \text{ mM}$, $C_{\text{TEGO IL K5}} = 100 \text{ g L}^{-1}$

Prediction for four linear, aliphatic ketones as substrates with $C_{\text{Ketone}} = 30 \text{ mM}$.

Conditions:
 $m_{\text{LbADH}} = 1.0 \text{ mg}$, $m_{\text{GDH}} = 4.2 \text{ mg}$,
 $C_{\text{NADPH}} = 0.1 \text{ mM}$, $C_{\text{Glucose}} = 200 \text{ mM}$,
 $C_{\text{Ketone}} = 30 \text{ mM}$, $C_{\text{ADA-buffer}} = 150 \text{ mM}$,
 $C_{\text{TEGO IL K5}} = 100 \text{ g L}^{-1}$, $C_{\text{H}_2\text{O}_2} = 10 \text{ mM}$,
 $\text{pH} = 7.5$, $\tau = 3.75 \text{ h}$, $dV/dt = 4.0 \text{ mL/h}$

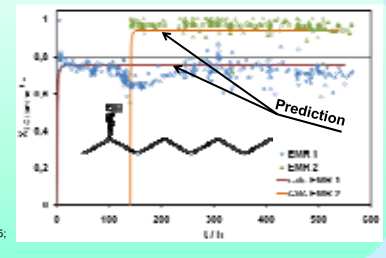


Synthesis of (*R*)-2-Octanol in a cascade of two EMR

Synthesis

Results	EMR 1	EMR 2
$\text{TON}_{\text{LbADH}} / 10^6$	22.9	6.10
$\text{TON}_{\text{GDH}} / 10^6$	5.20	1.39
$\text{TON}_{\text{NADP}^+}$	435	144
$\text{STY}/\text{mmol}\cdot\text{L}^{-1}\cdot\text{d}^{-1}$	272	97
ee	> 99.9	

Conditions:
 $m_{\text{LbADH}} = 1.0 \text{ mg}$ /per reactor, $m_{\text{GDH}} = 4.2 \text{ mg}$ /per reactor,
 $C_{\text{NADPH}} = 0.1 \text{ mM}$, $C_{\text{Glucose}} = 200 \text{ mM}$, $C_{\text{2-Octanone}} = 60 \text{ mM}$,
 $C_{\text{ADA-buffer}} = 150 \text{ mM}$, $C_{\text{TEGO IL K5}} = 100 \text{ g L}^{-1}$, $C_{\text{H}_2\text{O}_2} = 20 \text{ mM}$, $\text{pH} = 7.5$,
 $\tau = 3.75 \text{ h}$, $dV/dt = 4 \text{ mL/h}$

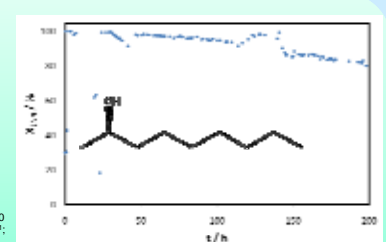


Synthesis of (*R*)-2-Nonanol in a single EMR

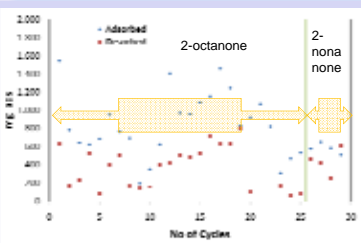
Synthesis

Results	
$\text{TON}_{\text{LbADH}} / 10^6$	3.6
$\text{TON}_{\text{GDH}} / 10^6$	0.82
$\text{TON}_{\text{NADP}^+}$	552
$\text{STY}/\text{mmol}\cdot\text{L}^{-1}\cdot\text{d}^{-1}$	350
ee	> 99.9

Conditions:
 $m_{\text{LbADH}} = 1.0 \text{ mg}$, $m_{\text{GDH}} = 4.2 \text{ mg}$, $C_{\text{NADPH}} = 0.1 \text{ mM}$, $C_{\text{Glucose}} = 200 \text{ mM}$, $C_{\text{2-Nonanone}} = 33 \text{ mM}$, $C_{\text{ADA-buffer}} = 150 \text{ mM}$, $C_{\text{TEGO IL K5}} = 100 \text{ g L}^{-1}$,
 $C_{\text{H}_2\text{O}_2} = 10 \text{ mM}$, $\text{pH} = 7.5$, $\tau = 5.5 \text{ h}$, $dV/dt = 2.7 \text{ mL/h}$



Down Stream Processing & Recycling



Add fresh ketone, NADP⁺ and Glucose

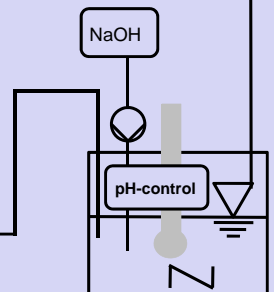
GC-Analysis

The product solution is pumped through the column filled with SPE-material. The product adsorbs on the material and is subsequently eluted with *n*-Heptane.



Stainless steel column filled with 4.4 g SPE-material HR-P (Macherey-Nagel)

The product-solution coming from the reactor has a pH of ~6.5. Before recycling the reaction, pH has to be re-adjusted to the initial value of 7.5.



Conclusions

- ✓ An ionic solubiliser (TEGO IL K5, Evonik Goldschmidt) is available to increase the ketone-solubility
- ✓ Both enzymes are stable under process conditions, high conversions and TON were achieved.
- ✓ The SPE-material is stable for more than 25 cycles with different substrate/product-pairs.
- ✓ It is possible to recycle the reaction mixture and though decrease the E-factor ($\text{kg}_{\text{waste}} / \text{kg}_{\text{product}}$) by a factor of 10, from 130 to 13
- ✓ The use of a reactor cascade is favorable compared to a single reactor
- ✓ A Michaelis-Menten based model is available to describe the EMR

Outlook

- Automate the whole setup
- Transfer the concept to different substrates
- Establish the product elution with supercritical CO₂

Acknowledgement: Prof. Dr. Marcel Liaw (RWTH Aachen), Macherey Nagel for the supply of the SPE-material, Kerstin Hell and Dr. Peter Schwab (Evonik Goldschmidt) for providing TEGO IL K5, and X-Zyme GmbH for providing LbADH and GDH

Literature:

- General:
- [1] S. Leuchs, L. Greiner, Alcohol Dehydrogenase from *Lactobacillus brevis*: A Versatile Robust Catalyst for Enantioselective Transformations Chemical & Biochemical Engineering Quarterly, 2011, 25, 267-281
 - [2] E. Thurman, M. Mills, Solid-Phase Extraction - Principles and Practice, John Wiley, 1998
 - [3] Solid Phase Extraction Application Guide, Macherey Nagel, 2009

Related work:

- [4] C. Kohlmann, S. Leuchs, L. Greiner, W. Leitner, Continuous Biocatalytic Synthesis of (*R*)-2-Octanol with Integrated Product Separation, Green Chemistry, 2011, 13, 1430-1436
- [5] C. Kohlmann, N. Roberz, S. Leuchs, Z. Dogan, S. Lütz, S. Nörmann, L. Greiner, Ionic liquid facilitates biocatalytic conversion of hardly water soluble ketones, Journal of Molecular Catalysis B: Enzymatic, 2011, 68, 147-153