

Determination of mixing efficiency of micro structured mixers by isothermal heat balance calorimetry

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Funded by: BMWi via AIF
Period: 01.05.2012 - 30.04.2014



Project idea

Use the enthalpy of mixing ($h_{E,id}$) as a reference point for determination of mixing efficiency (G) of micro mixing devices

$$G = h_{E,eff} / h_{E,id}$$

- $h_{E,id}$
- Measure for ideal mixing of two fluids on molecular scale
 - Available in databases
 - Accessible by isothermal calorimetry

- $h_{E,eff}$
- Obtained from continuous heat balance calorimetry for the case when mixing takes place inside a micro mixing device

Benefits

- No need for optically transparent devices
- No need for knowledge of mixer channel geometry
- Well defined reference point / High reproducibility
- Possible wide variation of fluid viscosity

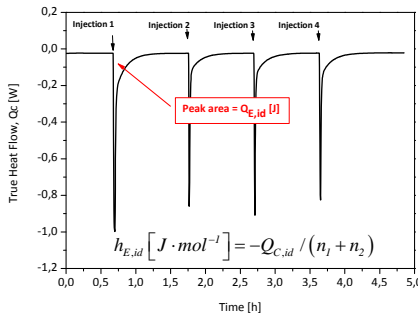
Types of experiments

ChemiSens CPA202 reaction calorimeter - "true heat flow" principle

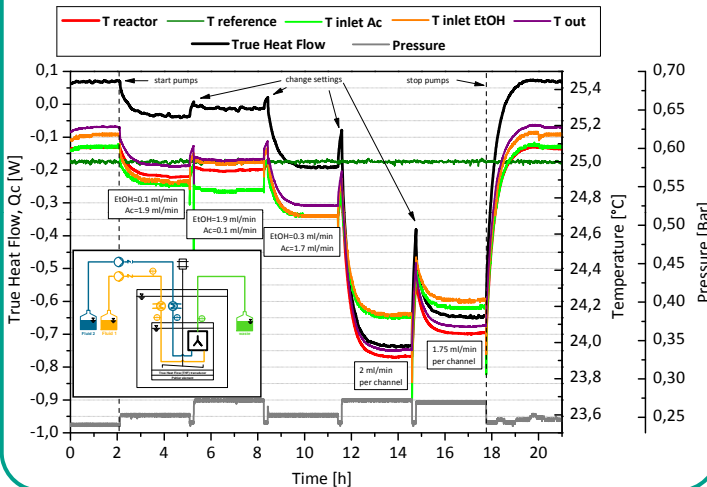
BATCH / $h_{E,id}$

Model substances
ethanol / acetone

Reference point
T = 25 °C
Heat transfer loop
22 ml
Injection syringe pump



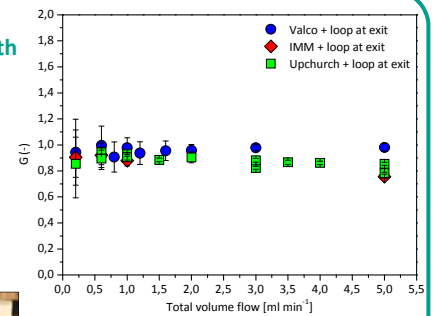
CONTINUOUS / $h_{E,eff}$



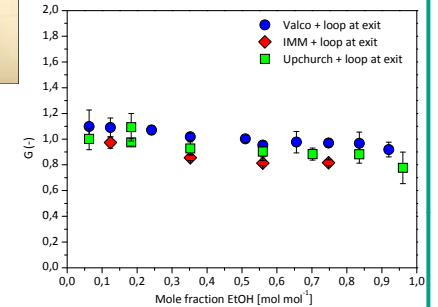
Mixer characterisation

Reference point ($h_{E,id}$; $G=1$)
determination \Rightarrow mixer with residence coil at exit

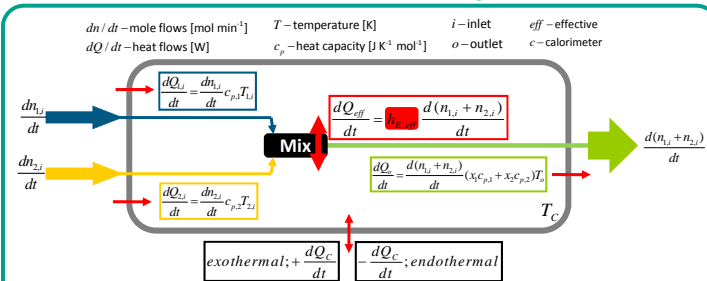
- Continuous experiments
- EtOH / Ac = 1 / 1
- T(reactor) = 25 °C
- Stirrer = 500 rpm



- Continuous experiments
- F(total) = 2 mL min⁻¹
- T(reactor) = 25 °C
- Stirrer = 500 rpm



Heat balance of continuous mixing

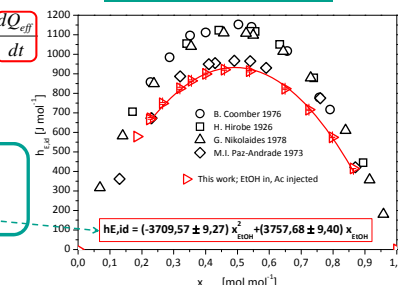


Heat flow balance

$$0 = \left(\frac{dQ_{1,i}}{dt} + \frac{dQ_{2,i}}{dt} - \frac{dQ_{3,o}}{dt} - \frac{dQ_C}{dt} + \frac{dQ_{eff}}{dt} \right)$$

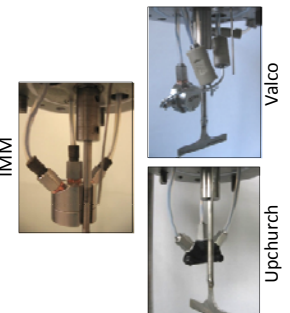
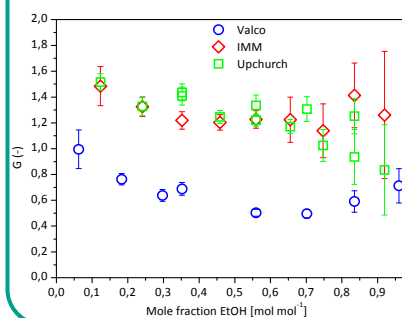
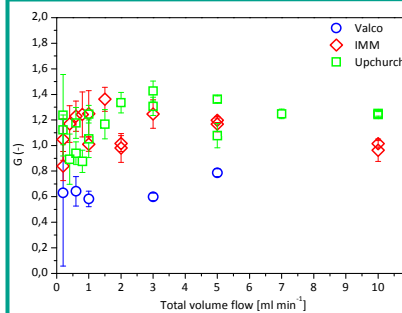
$$G = \frac{h_{E,eff}}{h_{E,id}} = \frac{\frac{dQ_{eff}}{dt} \cdot \frac{d(n_{1,i} + n_{2,i})}{dt}}{\frac{dQ_C}{dt}}$$

Polynomial fit of batch data



Net performance of mixer (without residence coil)

- Continuous experiments
- EtOH / Ac = 1 / 1
- T(reactor) = 25 °C
- Stirrer = 500 rpm



- Continuous experiments
- F(total) = 2 mL min⁻¹
- T(reactor) = 25 °C
- Stirrer = 500 rpm

Summary

- G is suitable for experimental determination of mixing efficiency
- $h_{E,id}$ is accessible continuously
- Preliminary results: A. Pashkova, L. Greiner *Chem. Eng. Sci.* 76 (2012) 45-48

Outlook

- Identify reasons for deviation of G
- Variation of fluid viscosity
- Test of reactive systems (acid/base)
- Change mixer types / peripherals
- Dimension analysis